## WASTE STABILIZATION PONDS 6 Maturation ponds

1.	Image: Natural Wastewater Treatment & Reuse   Image: Natural Wastewater Treatment & Reuse	This presentation is on maturation ponds, and these are the third type of pond that we commonly use.
2.	Waste Stabilization Ponds in Series Why? Different ponds have different functions BOD removal poor in maturation ponds, but faecal bacterial removal is high Theory indicates that a series of small ponds outperforms a single pond of same overall size also observed in practice	We use ponds in <b>series</b> because different pond types have different functions. BOD removal is good in anaerobic and facultative ponds, but poor in maturation ponds, which tend to be used for the removal of faecal bacteria and other excreted pathogens. We know from theory, and we can observe this in practice as well, that a series of small ponds outperforms a single pond of the same overall size.
3.	<ul> <li>So, either (a) - which is better         <ul> <li>A + F + M + M + M + M + M + M + M + M + M</li></ul></li></ul>	So we have either series (a) shown on the slide or series (b), and there's a preference for series (a) as BOD removal in anaerobic ponds is so good. The size and number of maturation ponds depends on the final effluent quality we need to produce; and for maximal performance the maturation ponds should all be the same size. This may not, of course, be possible, but at this, the process, stage of the design we assume that it is.

4.	E. coli removal in WSPMarais' method:assumes first-order kinetics in a completely mixed reactor: $N_e = N_i/(1 + k_{B(T)}\theta)$ $N_e = N_i/(1 + k_{B(T)}\theta)$ $E. coli$ value of $k_B$ is strongly temp. dependent: $k_{B(T)} = 2.6(1.19)^{T-20}$	We normally design maturation ponds for <i>E. coli</i> removal, although of course we might in any one case want to design them for something else – nitrogen removal, for instance. We use the design method developed by the late Professor Marais: the first equation on the slide is the usual first-order equation for, in this case, <i>E. coli</i> removal in a completely mixed reactor; and the second equation is Marais' empirical equation for the variation of the first-order rate constant for <i>E. coli</i> removal, <i>k</i> <sub>B</sub> , with temperature, and its value is strongly temperature-dependent, changing by 19% for every 1 degC change in temperature.
5.	So, for a series of ponds: $N_i \rightarrow A \rightarrow F \rightarrow M_i - M \rightarrow N_e$ $N_e = \frac{N_i}{(1 + k_B \theta_{an})(1 + k_B \theta_{fac})(1 + k_B \theta_{mal})^n}$ • $N_i$ known, or can be measured; or take as 5 × 10 <sup>7</sup> per 100 ml • $N_e$ known (required effluent quality) • $\theta_{an} \& \theta_{fac}$ known, but $\theta_{mat}$ and n are both unknown	So for a series of ponds, and remembering that the effluent of one pond is the influent to the next, we can derive the equation for $N_e$ shown on the slide. This basically says that $N_e$ , the number of <i>E. coli</i> per 100 ml of the final effluent equals $N_i$ , the number per 100 ml of the raw wastewater, divided by a term for the anaerobic pond, by one for the facultative pond, and by one for the maturation ponds raised to the power <i>n</i> , where <i>n</i> is the number of maturation ponds. Now $N_i$ is either known or taken as, for example $5 \times 10^7$ per 100 ml; $N_e$ is known as it's the final effluent quality we need; and, at this stage in the design, we will have already designed the anaerobic and facultative ponds, so the retention times in these, $\theta_{an}$ and $\theta_{fac}$ , are also known.
6.	$\begin{split} N_{e} &= N_{i} / \left[ (1 + k_{B} \theta_{an}) (1 + k_{B} \theta_{fec}) (1 + k_{B} \theta_{mat})^{n} \right] \\ \text{so: } \underline{one equation, two unknowns:} \\ &= \text{either trial \& error - for example, try} \\ 2 \text{ ponds } @ 7 \text{ days, or 3 ponds } @ 5 \text{ days,} \\ &= \text{and see if } N_{e} \text{ is < required effluent value} \\ &= \text{ or } (\underline{and this is better}) \text{ calculate the value} \\ &= \text{ of } \theta_{mat} \text{ for } n = 1, \text{ then for } n = 2 \text{ etc. until} \\ \theta_{mat} < \theta_{mat}^{min} \end{split}$	So we have one equation with two unknowns. We can solve it either by trial and error, or (and this is better) by calculating the value of $\theta_{mat}$ for $n = 1$ , then for $n = 2$ , and so on until $\theta_{mat}$ is $< \theta_{mat}^{min}$ , the minimum value of $\theta_{mat}$ .

7.	□θ <sup>min</sup> : minimum value of θ <sub>mat</sub> , in range 3–5 days. A min. value is assigned to prevent algal washout and reduce hydraulic short-circuiting. Marais recommends 3 days in warm climates (~5 days in temperate climates)	A minimum value of $\theta_{mat}$ is used in order to minimize hydraulic short-circuiting and the allow sufficient time for the algae to multiply. $\theta_{mat}^{min}$ has a value in the range 3–5 days: generally 3 days in hot climates and 5 days in temperate climates.
8.	$ \begin{array}{ c c } \hline \theta_{mat}^{min}: \mbox{ minimum value of } \theta_{mat}, \mbox{ in range } \\ \hline 3-5 \ days. A \ min. \ value \ is \ assigned \ to \\ prevent \ algal \ washout \ and \ reduce \\ hydraulic \ short-circuiting. \ Marais \\ recommends \ 3 \ days \ in \ warm \ climates \\ (~5 \ days \ in \ temperate \ climates) \\ \hline Solution \ to \ equation \ might \ be, \ for \ example: \\ n = 1 \qquad \theta_{mat} = 150 \\ n = 2 \qquad \theta_{mat} = 20 \\ n = 3 \qquad \theta_{mat} = 4.2 \\ n = 4 \qquad \theta_{mat} = 1.6 \ \dots \ STOP! \\ \end{array} $	So when we solve the equation for $n = 1$ , $n = 2$ , and so on, we might get the following results: For $n = 1$ , $\theta_{mat} = 150$ days; for $n = 2$ , $\theta_{mat} = 20$ days; for $n = 3$ , $\theta_{mat} = 4.2$ days; and for $n = 4$ , $\theta_{mat} = 1.6$ days. We would <b>stop</b> here as the last calculated value of $\theta_{mat}$ is $< \theta_{mat}^{min}$ .
9.	<ul> <li>(a) Ignore values of θ<sub>mat</sub> &gt; θ<sub>fac</sub> and &lt; θ<sup>min</sup><sub>mat</sub></li> <li>(b) Choose the combination that requires least land (ie, the one for which the product of n and θ<sub>mat</sub> is smallest)</li> <li>&gt; include in this comparison the combination of θ<sup>min</sup><sub>mat</sub> and value of n for which θ<sub>mat</sub> first goes below θ<sup>min</sup><sub>mat</sub> (n = 4 in above example, for which θ<sub>mat</sub> = 1.6 d)</li> </ul>	So how do we interpret these results? Well, we would ignore values of $\theta_{mat} > \theta_{fac}$ (there's no theoretical basis for this, just 'engineering judgement'), and we obviously ignore values of $\theta_{mat} < \theta_{mat}^{min}$ . We then choose the combination of <i>n</i> and $\theta_{mat}$ that requires the least land – that is to say, the combination for which the product $n\theta_{mat}$ is a minimum, and we would include in this comparison the combination of $\theta_{mat}$ and the value of <i>n</i> for which the value of $\theta_{mat}$ first goes below $\theta_{mat}^{min}$ .
10.	$\begin{array}{l} \mbox{Therefore: 1. } \theta_{mat} \neq \theta_{fac} \\ \mbox{${\cal B$ut also:}$} \\ \mbox{${\cal B$ut also:}$} \\ \mbox{${\cal B$ut also:}$} \\ \mbox{${\cal B$ob loading constraint:}$} \\ \mbox{${\cal A$}_{s(M1)}$} \\ \mbox{${\cal B$ob loading constraint:}$} \\ \mbox{${\cal A$}_{s(M1)}$} \\ \mbox{${\cal A$}_{s(M1$	Thus $\theta_{mat}$ can't be greater than $\theta_{fac}$ , nor less than $\theta_{mat}^{min}$ . But we should also consider a BOD loading constraint: clearly the BOD loading on the first maturation pond can't be greater than that on the preceding facultative pond, and it's better if it's quite a bit less than this; and I prefer to say that the loading on M1 can't be more than 75% of the fac. pond loading. To calculate $\lambda_{s(M1)}$ we first determine the
		effluent BOD from the fac. pond by using the first-order equation for <i>unfiltered</i> BOD removal with $k_1 = 0.1 \text{ day}^{-1}$ (or, if it's a primary fac. pond, with $k_1 = 0.3 \text{ day}^{-1}$ ).

11.	In fact simplest to consider constraint # 3 first: $\theta_{M1} = 10L_iD/0.75\lambda_{s(fac)}$ [as $\lambda_s = 10L_iQ/A = 10L_iQD/AD = 10L_iD/\theta$ ] and follow the 4-step procedure $\rightarrow$	In fact it's best to consider this loading constraint first and, using the equation on the slide, determine the minimum value of $\theta_{M1}$ , and then follow the four-step procedure which I'll now describe.
12.	Maturation Pond Design Four-step procedureStep 1: Calculate: $\Theta_{M1}^{min} = 10L_iD/0.75\lambda_{s(fac)}$ $\downarrow \rightarrow = L_{e(fac)}$ 	The first step is the calculation of $\theta_{M1}^{min}$ , using the loading equation we've just derived.
13.	Step 2: Calculate retention time in second & subsequent maturation ponds: $\theta_m = \{ [N_p/N_e(1+k_B\theta_a)(1+k_B\theta_{M1})]^{1/n} - 1 \}/k_B \}$ now the retention time in M2, M3 etc. Solve for n = 1, 2, 3 etc. and STOP when $\theta_m < \theta_m^{min}$ (3-5 days) - assume this happens when n = ñ	Step 2 is to calculate the retention time in the second and subsequent maturation ponds, using the equation we had before but now, as shown on the slide, with a term for M1. We solve this equation for $n = 1$ , then for $n = 2$ , and so on until $\theta_{mat}$ is $< \theta_{mat}^{min}$ . Note that n is now the number of the second and subsequent ponds; it does not include M1.
14.	Step 3: Choose most appropriate combination* of $\theta_{mat}$ and n, <u>including</u> $\theta_{mat}^{min}$ and ñ * ie, the one for which their product is a MINIMUM, as this gives the least land area requirement	Step 3 is the selection of the most appropriate combination of $\theta_{mat}$ and <i>n</i> , including $\theta_{mat}^{\min}$ and $\tilde{n}$ , where $\tilde{n}$ is the value of <i>n</i> for which $\theta_{mat}$ first goes below $\theta_{mat}^{\min}$ .

15.	Step 4: Determine mat. pond areas taking net evaporation into account: Eqn for fac. ponds: $\theta_f = 2A_fD/(2Q_i - 0.001eA_f)$ Rearrange this for mat. ponds: $A_m = 2Q_i\theta_m/(2D + 0.001e\theta_m)$	Step 4 is the calculation of the maturation pond areas, taking net evaporation into account. With facultative ponds we had the first equation shown on the slide, and for maturation ponds we need to rearrange this equation in terms of $A$ , in fact $A_{\rm m}$ as shown in the second equation on the slide.
16.	<ul> <li>Design Temperatures</li> <li>For anaerobic &amp; facultative ponds: Des. temp. = mean temp. of coldest month</li> <li>For maturation ponds: Des. temp. = mean temp. of coolest month in the irrigation season</li> </ul>	Now a word on design temperatures. For anaerobic and facultative ponds we have to use the mean temperature of the coldest month, as the ponds have to function properly at this lowest mean monthly temperature. With maturation ponds it's less straightforward. If we were designing them for nitrogen removal, then we'd have to use the mean temperature of the coldest month; but if we're designing them to produce an effluent suitable for agricultural reuse, then we'd use the mean temperature of the coldest month in the irrigation season.
17.	N <sub>e</sub> = N <sub>i</sub> / [(1+ k <sub>B</sub> θ <sub>an</sub> )(1+ k <sub>B</sub> θ <sub>fac</sub> )(1+ k <sub>B</sub> θ <sub>mat</sub> ) <sup>n</sup> ] But should <u>same</u> value of k <sub>B</sub> be used for anaerobic, facultative and maturation ponds? Probably not, but not too much data available -in facultative ponds k <sub>B</sub> seems to be a function of organic loading as well as of time and temperature:	Going back to the design equation for <i>E</i> . <i>coli</i> removal in a series of ponds: it has to be asked whether we should use the same value of $k_B$ in all three types of pond. The answer is probably not, but we don't have too much data to say one way or the other, at least with any degree of confidence. But we do know that the equation is perfectly OK for a whole series of ponds, rather than for individual anaerobic, facultative or maturation ponds. In fac. ponds the value of $k_B$ seems to be a function of the BOD loading on the pond, as well as of time and temperature,
18.	Facultative ponds, Northeast Brazil, 25°C	as shown in this slide for a primary facultative pond in northeast Brazil, which had a mean in-pond temperature of ~25°C. The value of $k_{\rm B}$ decreased fairly linearly with BOD loading in the range 200–400 kg per ha per day; thereafter it remained essentially constant.

19.	$\begin{tabular}{ c c c c c c c c c c c c c c c c c c c$	This slide shows the performance of a series of five ponds in northeast Brazil in the late 1970s. The anaerobic pond had a retention time of nearly a week, much too long really, <sup>[*]</sup> and the facultative and the three maturation ponds had retention times of ~5.5 days. Most of the BOD and SS were removed, as would be expected in the anaerobic pond, and the SS actually increased in the fac. pond – due to the
	* See the presentation on anaerobic ponds for further details.	growth of the algae; but the truly remarkable performance of the series is the removal of faecal coliform bacteria, more or less by an order of magnitude in each pond, down to 30 per 100 ml in the final effluent – a better bacteriological quality than the water most people in developing countries have to drink. But the real point of results like these is that you can design a pond system to do more or less whatever you want. Pond systems are <i>flexible</i> .
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